AMENDMENTS TO THE SPECIFICATION

Please insert the following paragraph as the first paragraph of this application, immediately following the title:

This application is a continuation of U.S. Application Serial No. 09/414,002, now abandoned, which is a divisional of U.S. Application Serial No. 08/887,766, now U.S. Patent No. 6,023,005.

Please replace the paragraph beginning at page 11, line 9 with the following paragraph:

A preferred embodiment of a riser reactor configuration 10 for use in the present invention is depicted in Figure 1. A methanol feed 12 is at least partially vaporized in a preheater (not shown). The methanol feed is mixed with regenerated catalyst 28 and coked catalyst 22 at the bottom of the riser reactor 14. An inert gas and/or steam may be used to dilute the methanol, lift the catalyst streams 22 and 28, and keep pressure instrument lines clear of catalyst. This inert gas and/or steam mixes with the methanol and catalyst in the reactor 14. The reaction is exothermic, and the preferred reaction temperature, in the range of from about 300°C to about 500°C, is maintained by removing heat. Heat can be removed by any suitable means, including but not necessarily limited to cooling the reactor with a catalyst cooler (not shown), feeding some of the methanol as a liquid, cooling the catalyst feed to the reactor, or any combination of these methods.